Development and uniformity evaluation of low-dose medicated chewing gums prepared by compression method

Vývoj a hodnocení stejnoměrnosti žvýkacích gum s nízkou dávkou léčiv připravených lisováním

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Summary

The aim of this work was to develop medicated chewing gums (MCGs) containing 10 mg of lysozyme hydrochloride (LH) and 20 mg of ascorbic acid (AsA) obtained by the compression method with Health in Gum® (HiG®) PWD 01 as a compressible gum base. Because of a low content of active ingredients, it was essential to choose the way of adding them to the tableting mass and evaluate their distribution homogeneity in the dosage units. The blends for compression were prepared by two methods: the first one was simple mixing of all components; the second one included the step of wet granulation of a three-component mixture – LH, sucralose and a taste additive. Flow properties of LH, AsA, HiG®, LH granules and blends for compression were studied. MCGs were evaluated according to Ph.Eur. 9.0 Chapters 2.9.5, 2.9.6 and 2.9.40. AsA and HiG® were characterized as free flowing, while LH had insufficient flow properties. Compared with a simple mixed blend, the granulation step allowed significantly improving flow properties of the final blend for compression. Unlike MCGs compressed from the simple mixed blend, MCGs prepared through the granulation step met Ph.Eur. 9.0 Chapter 2.9.40 requirements. The propriety of MCG preparation method involving the step of wet granulation also has been confirmed by mass and drug content uniformity tests.

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Souhrn

Cílem této práce bylo vyvinout léčivé žvýkací gumy (MCG) obsahující 10 mg lysozyme-hydrochloridu (LH) a 20 mg kyseliny askorbové (AsA) získané lisováním se stlačitelným základem pro žvýkací gumy Health in Gum® (HiG®) PWD 01. Vzhledem k nízkému obsahu aktivních složek bylo nezbytné zvolit způsob jejich zapracování do tohoto základu a zhodnotit jejich distribuční homogenitu v dávkových jednotkách. Směsi pro lisování byly připraveny dvěma způsoby: prvním bylo jednoduché smíchání všech složek; druhý zahrnoval krok vlhké granulace třísložkové směsi – LH, sukralosa a chuťové přísady. Byly studovány tokové vlastnosti LH, AsA, LH granulátu a lisovacích směsí. MCG byly hodnoceny podle Ph.Eur. 9.0 kapitoly 2.9.5, 2.9.6 a 2.9.40. AsA a HiG[®] byly charakterizovány jako volně tekoucí, zatímco LH vykazoval nedostatečné tokové vlastnosti. Ve srovnání se směsí pro přímé lisování, krok granulace umožnil podstatně zlepšit tokové vlastnosti konečné lisovací směsi. Na rozdíl od žvýkacích gum připravených přímým lisováním, MCG připravené vlhkou granulací splňovaly požadavky Ph.Eur. 9.0 kapitoly 2.9.40. Vhodnost metody přípravy MCG zahrnující krok vlhké granulace byla také potvrzena výsledky hmotnostní a obsahové stejnoměrnosti.

Klíčová slova: léčivé žvýkací gumy • lysozym-hydrochlorid • kyselina askorbová • hmotnostní stejnoměrnost • obsahová stejnoměrnost • stejnoměrnost dávkových jednotek

Introduction

One of the key factors primarily affecting the choice of medication for many patients is the type of dosage form. As it is known, solid dosage forms for oral administration are the most convenient and preferable. Among modern solid oral dosage forms, medicated chewing gums

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(MCGs) offer valuable advantages such as easy and pleasant administration, suitable consumption at any time without need of water and swallowing, as well as very fast onset of action due to the oral mucosa absorption and therefore less first-pass metabolism¹⁻³).

Owing to a comparatively long retention time in the oral cavity, MCGs are attractive dosage form for the use in dentistry⁴⁻⁶⁾. Depending on active ingredients which incorporated into MCGs can exert a therapeutic or disease-preventive action on both soft oral tissues and dentin. In particular, MCGs can be a good delivery platform for releasing drugs against such common oral diseases as gingivitis, periodontitis, stomatitis and dental caries. A good candidate for medicated chewing gum formulation is lysozyme - a natural antimicrobial compound normally occurring in human saliva. Lysozyme possesses activity against gram-positive and some gramnegative pathogenic bacteria, fungi and viruses and has anti-inflammatory and immunomodulating effects⁷⁻⁹. It also serves as a protective agent violating the ability of microorganisms to be attached to a tooth surface that is caries prevention¹⁰⁻¹¹). Lysozyme hydrochloride (LH), a derivative of lysozyme, is known to be an active ingredient of several marketed medications (Lysobact[®], Bosnalijek, Bosnia and Herzegovina; Lysopain® N, Sanofi-Aventis, Switzerland; Glossithiase[®], Jolly-Jatel, France; etc.), in which its dose per intake varies from 5 to 20 mg.

Other oral problems which can be cured by MCGs are hyposalivation and xerostomia, experienced as mouth dryness. Inadequate saliva production reduces the defence mechanisms of the oral cavity, significantly increasing the risk of oral mucosa diseases, oral ulcers and inflammation symptoms. Administration of MCGs directly increases salivation in response to mechanical (chewing) stimulus¹²⁾. In addition to chewing, salivary flow can be enhanced by using saliva stimulants – organic acids, e.g. ascorbic acid (AsA), which also plays a prominent role in oral health maintenance. AsA deficiency has been proved to cause dryness of oral mucosa, gingival bleeding and petechial hemorrhages in various parts of the mouth, resulting in xerostomia, ulcerative gingivitis and stomatitis development¹³⁾. However, it should be borne in mind that high concentrations of AsA may demineralize teeth, leading to dental erosions. In the view of this, low doses of AsA should be considered for inclusion in chewing products. For example, the amounts of AsA of 30 and 60 mg incorporated into MCGs were shown to be "too low to affect hard tissues"¹⁴).

There are three main methods for the production of MCGs: traditional (melting) method (I), cooling, grinding and tableting method (II), and direct compression method (III). The principal drawback of the first two methods is the difficulty to achieve high accuracy of content uniformity of active pharmaceutical ingredients (APIs) in MCGs. For instance, in the case of the most commonly used traditional method the heating process and further mixing of highly viscous mass lead to the risk of alterations in the shape, size and/or weight of

the final gums, which complicates the control of dosing homogeneity. Moreover, the melting technology is associated with raised temperatures, which may cause instability of thermosensitive ingredients, as well as with the use of complex equipment for hot melt processing and cooling. In contrast, the direct compression method allows not only simplifying and speeding up the manufacturing process of MCGs but also excluding the above-mentioned risks and drawbacks, especially by using directly compressible co-processed gum bases like Health in Gum[®] (HiG[®]) developed by Cafosa Gum SA (Spain)^{1-3, 15}).

Despite apparent advantages, the direct compression method is often associated with challenges. For instance, segregation of the components can occur, leading to inhomogeneous distribution of ingredients in the mass for compression and then in the dosage units. One of the principal risk factors for segregation is the wide range of particle sizes in the direct compression blends, in which APIs tend to have the finest particles. Besides, other powder properties, which are important for a successful compression process, such as good flowability, also depend a lot on particle size uniformity¹⁶.

Improving powder flowability is achieved when using a granulation technique that narrows particle size distribution and in such a way eliminates segregation problems. The most effective way to turn the powders into granules is by wetting powder blend with granulating liquid and further milling and drying the wetted mass, i.e. the-so called "wet granulation".

Although wet granulation provides apparent improvement of certain parameters, it requires more time and equipment units compared to direct compression and there is a risk of product loss during the different processing steps (granulation, drying, sieving). All of these factors can increase costs of the final product. Wet granulation is also contraindicated for moisture sensitive materials.

Thus, the aim of this work was to develop MCGs containing lysozyme hydrochloride 10 mg and ascorbic acid 20 mg obtained by the compression method using $HiG^{\text{@}}$ as the compressible gum base. Because of a low content of APIs, it was essential to choose the way of addition of APIs to the chewing gum mass. In the view of this, two batches of MCGs were prepared – by the direct compression method and with the step of wet granulation – and subjected to the evaluation of API distribution homogeneity in the dosage units.

Experimental part

Materials

Description of APIs and excipients used in the study is given in Table 1. All the chemicals and reagents used were of analytical grade.

Preparation of medicated chewing gums

Two batches of MCGs were obtained by different methods. To prepare the first MCG batch, all ingredients

were sieved through a sieve with a pore diameter of 1.0 mm, then dry-mixed and directly compressed (i.e., direct compression method) – batch DC. The second method included the step of wet granulation of the mixture of LH, a taste additive and sucralose. In this method, the three-component mixture was wetted using 96.0% ethanol, granulated through a sieve with a pore diameter of 2.0 mm, then dried at a room temperature and sifting through a sieve with a pore diameter of 1.0 mm. After that the granules were individually mixed with the rest of ingredients – batch WG. Both batches of MCGs were produced on a laboratory single-punch tablet press (model HTM-01E, Mariupol Plant of Technological Equipment, Ukraine) to obtain gums with a mass of 1000 mg.

The composition of the batches is given in Table 2.

Bulk and flow properties

To choose the proper method for gum mass preparation, bulk and flow properties of APIs, granules, $HiG^{\text{(B)}}$ and final blends for compression (batch DC and batch WG)

Table 1. Description of AF1s and exciptents used in the study							
Name of ingredient	Manufacturer	Country	Function in the MCG formulation				
Lysozyme hydrochloride	Bouwhuis Enthoven B.V.	Netherlands	Active pharmaceutical ingredient				
Ascorbic acid	Foodchem International Corporation	China	Active pharmaceutical ingredient				
Solo Sucralose Non-Micronised NF	V.B. Medicare Pvt. Ltd.	India	Intense sweetener				
Nat Apple Flavor Wonf	Kerry Inc.	Malaysia	Taste additive				
Apple FLV LQD FA-BO2980	Kerry Inc.	Malaysia	Flavor				
Syloid [®] 244FP	Grace GmbH & Co. KG	Germany	Moisture scavenger, carrier for liquid flavour, glidant				
Magnesium stearate	S.D. Fine Chemicals Ltd.	India	Lubricant				
Health in Gum [®] PWD 01	Cafosa Gum SA	Spain	Chewing gum base				

 Table 1. Description of APIs and excipients used in the study

Table 2. Composition of MCG batches obtained by the direct compression (DC) method and with a step of wet granulation (WG)

	Composition					
Batch designation	Ingredients	Amount, mg/per gum				
Batch DC	Lysozyme hydrochloride	10.0				
	Ascorbic acid	20.0				
	Solo Sucralose Non-Micronised NF	1.5				
	Nat Apple Flavor Wonf	20.0				
	Apple FLV LQD FA-BO2980	6.0				
	Syloid [®] 244FP	10.0				
	Magnesium stearate	15.0				
	Health in Gum [®] PWD 01	Up to 1000.0				
Batch WG	Intragranular:					
	Lysozyme hydrochloride	10.0				
	Solo Sucralose Non-Micronised NF	1.5				
	Nat Apple Flavor Wonf	20.0				
	96.0% ethanol	15.0				
	Extragranular:					
	Ascorbic acid	20.0				
	Apple FLV LQD FA-BO2980	6.0				
	Syloid [®] 244FP	10.0				
	Magnesium stearate	15.0				
	Health in Gum [®] PWD 01	Up to 1000.0				

such as bulk density, tapped density, compressibility index and Hausner ratio, flowability, and angle of repose were determined.

A Pharma Test Tap Density Tester (Model PT-TD1, Germany) was used to determine bulk and tapped densities of the samples as described in the European Pharmacopoeia (Ph.Eur.) 9.0 Chapter 2.9.34 "Bulk density and tapped density of powders". Compressibility index and Hausner ratio were calculated from bulk and tapped densities according Ph.Eur. 9.0 Chapter 2.9.36 "Powder flow".

Flowability was determined as the time required for pouring out of 100.0 g of the sample. Flow rate measurements were performed using a fixed conical funnel (diameter of the outflow opening, 15 mm) with a damper of a laboratory device for powder flowability determination (Model VP-12A, Mariupol Plant of Technological Equipment, Ukraine). The diameter of the cone formed by the heaped material was registered. Angle of repose was calculated as the inverse tangent (arctan) of the ratio of the cone maximum height to its radius.

Optical microscopy

A Konus 1000× Academy Biological Monocular Microscope (Konus Italia Group S.P.A., Italy) equipped with a camera ScopeTek was used for particle characterization of the samples. The processing of photos was carried out using Scope Photo software (version 3.0.12.498).

Evaluation of prepared MCGs

The prepared gums were evaluated according to Ph.Eur. 9.0 Chapters 2.9.5 "Uniformity of mass of single-dose preparations", 2.9.6 "Uniformity of content of single-dose preparations", and 2.9.40 "Uniformity of dosage units".

Assay

The LH assay was carried out spectrophotometrically using a Specord 200 spectrophotometer (Analytik Jena AG, Austria) as described in the Japanese Pharmacopoeia (JP XVII) monograph for LH. To perform the assay test, one gum was crushed to powder by using a laboratory crushing machine Knife Mill Pulverisette 11 (Fritsch GmbH, Germany) to obtain the sample solution with an approximate LH concentration of 0.01 mg/ml. Lysozyme JP Reference Standard (RS) (PMRJ, Japan) with 0.98 mg of lysozyme per mg (calculated on the dried basis) was used in this experiment to obtain the standard solution (approximate concentration, 0.01 mg/ml).

The AsA assay was performed by redox-based iodometric titration. One gum (previously crushed to powder) was placed into a flask and for better wetting of the powder 20 ml of 40.0% ethanol was added. The content of the flask was heated to 40–50 °C, shaken and then cooled to a room temperature. 10 ml of a 0.1 M hydrochloric acid solution, 0.5 ml of a 10 g/l potassium iodide solution, and 2 ml of a starch solution as the

indicator were added to the flask. The mixture was shaken and titrated with a 0.0167 M potassium iodate solution until a persistent violet-blue color was obtained. 1 ml of 0.0167 M potassium iodate is equivalent to 8.8271 mg of AsA.

Statistical analysis

Statistical analysis was carried out using Microsoft Excel 2010 software.

For the test "Uniformity of dosage units" (Ph.Eur. Chapter 2.9.40), the contents of AsA and LH were determined in each of 10 randomly selected MCGs of the batch. The acceptance value (AV) was calculated depending on the mean of individual contents (\bar{X} ,%) as described in Ph.Eur. The batch was considered to meet the requirements of this test if AV was less than or equal to the maximum allowed acceptance value L1 = 15.

For the test "Uniformity of mass of single-dose preparations" (Ph.Eur. Chapter 2.9.5) the average mass, SD, RSD, and RSD maximum level (RSD_{max}) were calculated. RSD_{max} was determined as $RSD_{max} = max\Delta_x/t(95, 19)$, where $max\Delta_x - maximum$ percentage deviation, t(95, 19) – Student's distribution at 95% confidence level and the degree of freedom of 19¹⁷). RSD calculated for this batch of MCGs was compared with RSD_{max}, which is 2.4 with $max\Delta_x = 5.0\%$ and t = 2.093.

For the test "Uniformity of content of single-dose preparations" (Ph.Eur. Chapter 2.9.6), the contents of LH and AsA were determined in each of 10 MCGs. For each individual MCG, the content of AsA in mg per a dosage unit $(Cmg_{/m_i})$, the percentage content of AsA with reference to the average content $(C_{\%/c})$, and the percentage content of AsA with reference to the nominal content $(C_{\%/c})$ were calculated using the formulas [1], [2] and [3], respectively:

$$Cmg_{/m_i} = \frac{V_T \cdot F \cdot 8.8271}{m_i},$$
[1]

$$C_{\%/\bar{c}} = \frac{C_{mg/m_i} \cdot 100}{\bar{c}},$$
[2]

$$C_{\%/C_{nom}} = \frac{C_{mg/m_i} \cdot 100}{C_{nom}},$$
 [3]

where V_T is the volume of 0.0167 M potassium iodate solution, ml; F is the titrant correction factor; m_i is the mass of one MCG unit, mg; \overline{C} and C_{nom} are the average content (mg) and the nominal content (mg) of AsA, respectively.

The obtained results were averaged by calculating the average values \bar{C}_{mg/m_l} , $\bar{C}_{\%/\bar{C}}$, $\bar{C}_{\%/C_{nom}}$, as well as the relative standard deviation values RSD_{mg/m_l} , $RSD_{\%/\bar{C}}$, $RSD_{\%/C_{nom}}$, and the relative confidence intervals Δ_{mg/m_l} , $\Delta_{\%/\bar{C}}$, $\Delta_{\%/\bar{C}_{nom}}$.

The evaluation of LH content uniformity in the dosage units was carried out in the same way as for AsA, wherein the amount of LH (mg) per 1 mg of MCG (C_{LH}) and the

$$C_{mg}_{/m_i} = \frac{M_S}{M_T} \times \left[\frac{(A_{S1} - A_T)}{(A_{S1} - A_{S2})} + 1\right] \times m_i$$
 [4]

where M_s – amount of Lysozyme RS taken (calculated on the dried basis), mg; M_T – amount of the sample taken (calculated on the dried basis), mg; A_{SI} and A_{S2} – the absorbance at 640 nm of the standard solutions with the concentrations of 0.005 mg/ml and 0.01 mg/ml, respectively; A_T – the absorbance at 640 nm of the sample solution; m_i – the mass of one MCG unit, mg.

Results and discussion

To find out whether it is possible to use direct compression for obtaining MCGs with LH and AsA, the bulk and flow properties of APIs and the gum base as the dominant excipient in the gum mass were studied (Table 3).

From Table 3, it is obvious that LH exhibited insufficient flow properties – it does not flow through the funnel at all and the values of compressibility index and

Hausner ratio indicate a passable flow character. Another situation was observed in the cases of AsA and gum base HiG® which were free-flowing with close average values of flow rate. Possible explanations of these findings may include several points. First, poor flow of LH powder can be associated with much finer particle size distribution compared to AsA and HiG®. As it is known, flowability is the capacity of powders to pour out and the driving force of this process is gravity, hence the greater the mass of powder particles, then the better their ability to flow. Obviously, LH powder had the smallest value of bulk density, since its particles are the lightest and their gravity was not enough to fill all cavities between them. When tapping was applied, additional force contributed to further particle downward movement and powder density changed dramatically resulting in a greater Hausner ratio. The second point is the difference in the surface character of the particles. If the powder particles have a rough, unsmooth surface, then they will form many bridges due to the cohesive bonds at the point of contact between one another under loose packing. Under tapping, these cohesive bonds are broken and again higher powder density is obtained. On the other hand, less cohesive powders will not undergo so much change

Table 3. Bulk and flow properties of APIs and the compressible gum base Health in Gum®

Parameters	Samples					
rarameters	LH	AsA	HiG [®] PWD 01			
Bulk density, g/cm ³	$0.586 \pm 0.002*$	$0.902 \pm 0.013 *$	$0.642 \pm 0.001 *$			
Tapped density, g/cm ³	$0.773 \pm 0.003*$	$1.120 \pm 0.013 *$	$0.737 \pm 0.002*$			
Compressibility index, %	24	19	13			
Hausner ratio	1.32	1.24	1.15			
Flowability, s/100 g	N/A	$7.90 \pm 1.09 \texttt{*}$	$7.45 \pm 0.38*$			
Angle of repose, °	N/A	$35.75 \pm 0.74*$	$29.26 \pm 1.61*$			
Flow character	passable	fair	good			

LH – lysozyme hydrochloride, AsA – ascorbic acid, N/A – not applicable, the powder does not flow *n = 5, p < 0.05, values are expressed as mean ± confidence interval

Table 4. Bulk and flow properties of lysozyme hydrochloride granules and two final blends

Demonstern	Samples					
Parameters	Granules of LH	Batch DC	Batch WG			
Bulk density, g/cm ³	$0.401 \pm 0.001*$	$0.705 \pm 0.007*$	$0.699 \pm 0.005 *$			
Tapped density, g/cm ³	$0.475 \pm 0.006*$	$0.847 \pm 0.009*$	$0.763 \pm 0.004 \texttt{*}$			
Compressibility index, %	15	17	8			
Hausner ratio	1.18	1.20	1.09			
Flowability, s/100 g	8.01 ± 0.62*	$8.95 \pm 0.58*$	$5.94\pm0.25*$			
Angle of repose, °	34.47 ± 1.48*	37.83 ± 1.02*	$27.65\pm0.87\texttt{*}$			
Flow character	good	fair	excellent			

LH - lysozyme hydrochloride

*n = 5, p < 0.05, values are expressed as mean \pm confidence interval

in bulk density, as they do not form the bridging cohesive bonds¹⁸).

However, it should be noted that the flow characters of AsA and HiG[®] slightly differ according to the calculated compressibility indexes and Hausner ratios, as well as angle of repose values, and are regarded as fair and good, respectively. These data are in accordance with the declared applicability of HiG[®] as a gum base intended for direct compression^{1, 3, 19}.

Taking into account insufficient flow properties of LH, which may cause its inhomogeneous distribution in MCGs¹⁶), two different methods for preparation of gum mass were tested. The first method was simple dry mixing of all ingredients as it is usually practiced in direct compression technology (batch DC). The second method included the step of wet granulation of a three-component mixture (LH, sucralose and taste additive). AsA was not considered to undergo wet granulation because of its satisfactory flow properties and also in order to avoid its oxidation upon contact with the granulating liquid²⁰). Therefore, AsA powder was mixed with the granules and gum base, after that the rest of the excipients were added (batch WG). Bulk and flow properties of LH granules

and blends for compression of two batches are given in Table 4.

As it is clearly seen from Table 4, the granulation step expectedly improved flow properties of LH and the blend for compression of the batch WG, whose flow character was achieved to be excellent contrary to the simple mixed blend of the batch DC with only fair flow. To determine how granulation step affects particle homogeneity in the blend for compression, we carried out optical microscopic examination for both blends (Fig. 1).

According to Fig. 1, it can be concluded that the step of wet granulation has led to more homogenous particles in the final blend for compression (batch WG), which also resulted in improving flow properties of this blend.

We further studied whether the method for preparation of the blend for compression is crucial for the uniformity of compressed chewing gums.

According to Ph.Eur. 9.0, MCGs should comply with the test for uniformity of dosage units (UDU), which characterizes the degree of distribution homogeneity of APIs among dosage units (chapter 2.9.40). For singledose solid dosage forms with multiple components, content uniformity test is applicable. This test is based

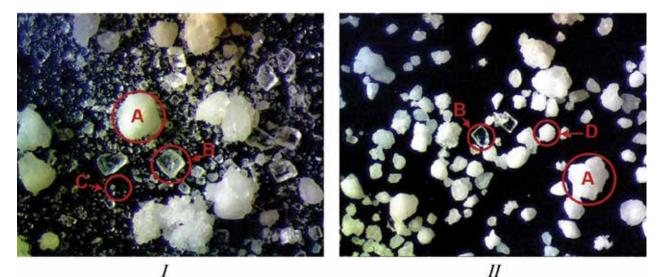


Fig. 1. Optical microscopy characterization (3.3 times zoom) of particles: I – simple mixed blend (batch DC), II – blend prepared with the step of wet granulation (batch WG), A – HiG[®] particles, B – ascorbic acid particles, C – lysozyme hydrochloride and the rest excipient particles, D – granules obtained from lysozyme hydrochloride, sucralose, and taste additive

API	<i>X</i> , %	<i>s</i> , %	RSD, %	AV	Ph.Eur. 2.9.40 requirements 15.0≥ <i>AV</i>
Batch DC					
AsA	93.00	16.09	17.30	44.11	_
LH	113.79	36.08	31.71	98.88	_
Batch WG					
AsA	100.31	2.06	2.05	4.92	+
LH	99.10	4.52	4.56	10.94	+

Table 5. The results of content uniformity test of dosage units for two batches of MCGs

on the assay of the APIs in each of 10 units of the dosage form to determine whether the individual contents are within the limits set²¹). Table 5 shows the results of content uniformity test of dosage units for MCGs of two different batches.

Since for batch DC MCGs acceptance values (AV) calculated for both APIs are significantly higher than L1 values, it was decided that further testing of 20 units (e.g., requirements of Ph.Eur. chapter 2.9.40) for this batch would not be appropriate.

Based on RSD and AV calculated for each API in MCGs of two different batches, it can be concluded that only batch WG dosage units meet requirements of Ph.Eur. 2.9.40 $L1 = 15.0 \ge AV$. So, further investigations were performed only for this batch of MCGs.

It is obvious that content uniformity is integral to mass uniformity of dosage units and critical deviations in drug content are often related to weight variations. In turn, weight variations can occur because of inadequate flow of

Sequence number

the blend for compression. Therefore, we have evaluated mass uniformity of batch WG MCGs in accordance with Ph.Eur. Chapter 2.9.5 "Uniformity of mass of single-dose preparations". The acceptance criterion in this test is a condition that not more than 2 of the individual MCG masses deviate from the average mass by more than \pm 5% and none deviates by more than \pm 10%. To ensure that each individual mass will be within established limits we also calculated RSD for this batch of MCGs and compared it with RSD_{max}, which was determined as mentioned above. The results of mass uniformity test are given in Table 6.

Taking into account the data of Table 6, MCGs of the batch WG meet the requirements of Ph.Eur. Chapter 2.9.5 "Uniformity of mass of single-dose preparations", since the deviation from the average mass for each of 20 dosage units does not exceed the acceptable value. Also, RSD calculated for this batch is less than RSD_{max} value.

Ph.Eur. 2.9.5 requirements

 $|\bar{m} - m_{i}|, \%$

Table 6. The results of mass uniformity of dosage units for MCGs of batch WG

m, mg

1 999.5 0.7 0.07 ++ 2 998.1 2.1 0.21 + 3 1000.9 -0.7 -0.07 + 4 1001.1 -0.9 -0.09 + 5 1000.9 -0.7 -0.07 + 6 997.5 2.7 0.27 + 7 998.7 1.5 0.15 + 8 1000.4 -0.2 -0.02 + 9 98.7 1.5 0.15 + 10 999.7 -0.25 -0.25 + 9 1002.7 -2.5 -0.25 + 10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 <th>of a MCG unit</th> <th></th> <th> m m_i , mg</th> <th> III III_i , /0</th> <th>i induit 21910 requirements</th>	of a MCG unit		m m _i , mg	III III _i , /0	i induit 2 1910 requirements
3 1000.9 -0.7 -0.07 + 4 1001.1 -0.9 -0.09 + 5 1000.9 -0.7 -0.07 + 6 997.5 2.7 0.27 + 7 998.7 1.5 0.15 + 8 1000.4 -0.2 -0.02 + 9 1002.7 -2.5 -0.25 + 10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 10	1	999.5	0.7	0.07	+
41001.1 -0.9 -0.09 $+$ 51000.9 -0.7 -0.07 $+$ 6997.52.7 0.27 $+$ 7998.71.5 0.15 $+$ 81000.4 -0.2 -0.02 $+$ 91002.7 -2.5 -0.25 $+$ 10999.5 0.7 0.00 $+$ 11997.5 2.7 0.27 $+$ 12996.1 4.1 0.41 $+$ 13999.2 1.0 0.10 $+$ 14998.1 2.1 0.21 $+$ 15 100.7 -1.5 -0.15 $+$ 16 1009.1 -8.9 -0.89 $+$ 17 1002.3 -2.1 -0.21 $+$ 18999.4 0.8 0.08 $+$ 20998.5 1.7 0.01 $+$ Average mass, \vec{n} , \vec{n} 2.8 \mathbf{KSD} , $\%$ 0.2841	2	998.1	2.1	0.21	+
51000.9 -0.7 -0.07 $+$ 6997.52.7 0.27 $+$ 7998.71.5 0.15 $+$ 8100.4 -0.2 -0.02 $+$ 91002.7 -2.5 -0.25 $+$ 10999.5 0.7 0.00 $+$ 11997.5 2.7 0.27 $+$ 12996.1 4.1 0.41 $+$ 13999.2 1.0 0.10 $+$ 14998.1 2.1 0.21 $+$ 15 100.7 -1.5 -0.15 $+$ 16 100.1 -8.9 -0.89 $+$ 17 102.3 -2.1 -0.21 $+$ 18999.4 0.8 0.08 $+$ 20998.5 1.7 0.01 $+$ Average mass, \vec{n} , \vec{n} 2.8 -3.4 -0.34 $+$ RSD, % 0.2841 -2.8 -2.8 -2.8 -2.8	3	1000.9	-0.7	-0.07	+
6 997.5 2.7 0.27 + 7 998.7 1.5 0.15 + 8 1000.4 -0.2 -0.02 + 9 1002.7 -2.5 -0.25 + 10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, mag 2.8	4	1001.1	-0.9	-0.09	+
7 998.7 1.5 0.15 + 8 1000.4 -0.2 -0.02 + 9 1002.7 -2.5 -0.25 + 10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, mg 100.2 - - + Standard deviation, s, mg 2.8 - - -	5	1000.9	-0.7	-0.07	+
8 1000.4 0.2 0.02 + 9 1002.7 -2.5 -0.25 + 10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m̄, mg 1000.2	6	997.5	2.7	0.27	+
9 1002.7 -2.5 -0.25 + 10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, mg 1000.2	7	998.7	1.5	0.15	+
10 999.5 0.7 0.00 + 11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 102.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, mg 1000.2	8	1000.4	-0.2	-0.02	+
11 997.5 2.7 0.27 + 12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m, mg 1000.2	9	1002.7	-2.5	-0.25	+
12 996.1 4.1 0.41 + 13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 102.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m̄ mg 1000.2 - - - Standard deviation, s, mg 2.8 - - -	10	999.5	0.7	0.00	+
13 999.2 1.0 0.10 + 14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m, mg 1000.2 - - - Standard deviation, s, mg 2.8 - - - RSD, % 0.2841 - - - -	11	997.5	2.7	0.27	+
14 998.1 2.1 0.21 + 15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m, mg 1000.2 - - - Standard deviation, s, mg 2.8 - - - RSD, % 0.2841 - - - -	12	996.1	4.1	0.41	+
15 1001.7 -1.5 -0.15 + 16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m, mg 1000.2 - - - Standard deviation, s, mg 2.8 - - -	13	999.2	1.0	0.10	+
16 1009.1 -8.9 -0.89 + 17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass , m, mg 1000.2 - - - Standard deviation, s, mg 2.8 - - -	14	998.1	2.1	0.21	+
17 1002.3 -2.1 -0.21 + 18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass , m, mg 1000.2 - - - Standard deviation, s, mg 2.8 - - - RSD, % 0.2841 - - - -	15	1001.7	-1.5	-0.15	+
18 999.4 0.8 0.08 + 19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass, m, mg 1000.2 - - - Standard deviation, s, mg 2.8 - - -	16	1009.1	-8.9	-0.89	+
19 1003.6 -3.4 -0.34 + 20 998.5 1.7 0.01 + Average mass , m, mg 1000.2 - - Standard deviation, s, mg 2.8 - - RSD, % 0.2841 - -	17	1002.3	-2.1	-0.21	+
20 998.5 1.7 0.01 + Average mass , m, mg 1000.2 -	18	999.4	0.8	0.08	+
Average mass, m, mg 1000.2 Standard deviation, s, mg 2.8 RSD, % 0.2841	19	1003.6	-3.4	-0.34	+
Standard deviation, s, mg2.8RSD, %0.2841	20	998.5	1.7	0.01	+
RSD, % 0.2841	Average mass, m, mg	1000.2		^ 	
	Standard deviation, s, mg	2.8			
RSD _{max} , % 2.4 2.4 > 0.2841 +	RSD, %	0.2841			
	RSD _{max} , %	2.4	2.4 >	0.2841	+

 $|\mathbf{m} - \mathbf{m}_i|, \mathbf{mg}$

The test of content uniformity of single-dose preparations (Ph.Eur. chapter 2.9.6) is also very important for single-dose preparations with a low content of API(s). This test is based on the assay of API(s) contents in a number of individual dosage units in order to determine whether the individual contents are within the limits set with reference to the average content of the sample²¹⁾. The nominal contents for LH and AsA are 10.0 and 20.0 mg per gum weighing 1000 mg, respectively, that is less than 2% of the total dosage unit mass for both APIs. The batch was considered to comply with the test if each individual content was between 85 and 115% of the average content²¹⁾.

The results of the test for uniformity of AsA content and LH content in 10 MCGs units of the batch WG are given in Tables 7 and 8, respectively.

The evaluation of AsA content uniformity in the MCG dosage units was carried out in two ways. Firstly, according to the requirements of Ph.Eur. 2.9.6, the percentage deviations of AsA content in the individual MCG units from its average content were compared with acceptable limits of 85–115% ($\Delta C \leq 15.0\%$). It should be noted that when testing according to Ph.Eur. 2.9.6 requirements, the value of the deviation from the nominal content is not taken into account. Secondly, the statistical parameters of the obtained results were compared with the critical values for these metrological characteristics (Table 7). The content of AsA in the MCG units is within 20.2 mg \pm 3.78% relative to its average content

and 20.0 mg \pm 3.78% relative to its nominal content, i.e. the deviation of the average content from the nominal content in the tested batch (100.94 – 100.00 = 0.94%) does not significantly affect the distribution of individual contents in single dose units and is within the acceptable limits in accordance with the requirements of Ph.Eur.

As it is seen from Table 8, the deviation of the average content of LH from its nominal content $\Delta = |10.0 - 10.05| = 0.05$ mg or |100.00 - 100.50| = 0.5 %.

Therefore, MCG batch WG meets the requirements of Ph.Eur. chapter 2.9.6 (Test A) – the content of APIs in each MCG unit is within the limits of 85-115% of the average content.

Content uniformity is one of the critical quality attributes of compressed solid dosage forms (tablets, MCGs, etc.) containing low doses of APIs. A number of factors, such as the concentration of individual components in the mixture for compression, particle shape and size distribution, bulk and flow properties, cohesive and adhesive characteristics of substances have a potential effect on this attribute. In addition, parameters of the technological process also have a certain impact on uniformity content: the intensity and duration of mixing, the shape and degree of loading of the mixer, etc.^{22, 23)}. For instance, the effect of mixing time and different low API concentrations on the content uniformity of directly compressed warfarin tablets was examined in the works of J. Muselík and colleagues^{22, 23)}, and also J. Elbl and colleagues²⁴⁾. According to their results, concentrations

Sequence number of a MCG unit	m _i , mg	V _T , ml	$C_{mg/mi}, mg$	С _{%/С} - %о	C ^{%/Cnon} , %0	$\Delta C = \overline{C} - \overline{C}_{mg/_{mi}} ,\%$	Ph.Eur. 2.9.6 requirements $\Delta C \le 15.0 \%$
1	999.5	2.30	20.3	100.61	101.56	-0.61	+
2	998.1	2.32	20.5	101.63	102.58	-1.63	+
3	1000.9	2.23	19.7	97.41	98.33	2.59	+
4	1001.1	2.34	20.6	102.20	103.16	-2.20	+
5	1000.9	2.30	20.3	100.47	101.41	-0.47	+
6	997.5	2.28	20.2	99.94	100.87	0.06	+
7	998.7	2.25	19.9	98.50	99.43	1.50	+
8	1000.4	2.23	19.7	97.46	98.38	2.54	+
9	1002.7	2.32	20.4	101.16	102.11	-1.16	+
10	999.5	2.30	20.3	100.61	101.56	-0.61	+
Averaged values	999.93		20.2	100.00	100.94		
s	1.6		0.3	1.67	1.69		
RSD, %	0.16		1.67	1.67	1.67		
RSD _{max} , %	6.6		1.67 < 6.6	1.67 < 6.6	1.67 < 6.6		+
$\Delta C_{\rm m/C}$			3.78	3.78	3.78		

Table 7. The results for the test of ascorbic acid content uniformity in 10 MCGs units of batch WG according to Ph.Eur. Chapter2.9.6

of API smaller than 2% per tablet did not allow to obtain, by the direct compression method, the products meeting the requirements of the Pharmacopoeia 2.9.6 and 2.9.40 even when using the optimized preparation and mixing technology.

Another study by M. T. am Ende and colleagues was devoted to the application of the granulation process (roller compaction) in the preparation of low-dose tablets. The use of this step was shown to minimize the segregation potential by improving content uniformity due to more homogeneous particle size distribution²⁵.

D. G. Morris and colleagues examined the influence of the excipient type and method of producing on the content uniformity of low-dose tablets. According to their conclusions, direct compression may be applicable for low-dose tablets (e.g. < 1 mg) when API has a suitable particle size and potency loss to equipment is negligible²⁶.

It should be noted that a principal difference between medicated chewing gums obtained by compression and common tablets is the presence of chewing gum base in the formulation, such as directly compressible HiG[®]. The possibility for obtaining MCGs by direct compression using this gum base is well described in other works^{27–29}, however, in those studies MCGs contain either one API that is easier to distribute in the blend for compression, or a higher content of API in the formulation. In the present study the principal ingredient of low-dose combination – HiG[®] PWD 01 – significantly differs from

the APIs in particle and technological properties, which do not allow obtaining by direct compression a uniform API content distribution in the final MCG batch. The solution proposed by us for this problem – preliminary wet granulation of the API with the finest particles – improved flow properties of the blend for compression and has led to MCGs which fully meet Ph.Eur. 2.9.6 and 2.9.40 requirements.

Thus, these findings confirm that unlike simple mixing the use of granulation technique for API having the finest particles, which are significantly smaller than the gum base HiG[®] particles, allows obtaining compressed MCGs with acceptable mass and drug content uniformity.

Conclusions

Compression method for the production of MCGs offers many advantages; however, some crucial issues similar to the tablet manufacture should be considered in this case. One of the most important of them is the achievement of weight and drug content uniformity in dosage units, directly affected by the blend for compression – its proper flow and absence of segregation caused by particle inhomogeneity. Our studies have demonstrated that the use of direct compression method for the production of low-dose combination MCGs does not allow obtaining dosage units with acceptable drug content uniformity. However, the use of granulation technique for API with the finest particles and insufficient

C^{%/Cnon}, C_{mg∕mi}, mg C %/c¯ % Ph.Eur. 2.9.6 Sequence number $\Delta C =$ m_i, mg of a MCG unit $|\overline{C}-\overline{C}_{mg/mi}|,\%$ requirements $\Delta C \leq 15.0$ % 1 997.5 9.9 98.51 99.00 1.49 +2 996.1 10.1 100.50 101.00 -0.50+ 3 999.2 97.51 9.8 98.00 2.49 +4 9.7 998.1 96.52 97.00 3.48 +5 1001.7 10.2 101.49 102.00 -1.49+6 1009.1 9.7 96.52 97.00 3.48 +7 1002.3 11.0 109.45 110.00 -9.45 +8 999.4 9.9 98.51 99.00 1.49 +9 1003.6 10.3 + 102.49 103.00 -2.4910 998.5 9.9 98.51 1.49 99.00 +1000.6 100.00 Averaged values 10.05 100.50 3.88 0.4 3.89 3.8 s RSD.% 0.38 3.88 3.88 3.88 RSD_{max},% 3.88 < 6.6 3.88 < 6.6 3.88 < 6.6 $^+$ 6.6 8.76 8.76 $\Delta C_{\%/c}$

Table 8. The results for the test of lysozyme hydrochloride content uniformity in 10 MCGs units of batch WG according to Ph.Eur.Chapter 2.9.6

flow not only improves flow properties of the blend for compression but also contributes to homogeneous drug content for both APIs in compressed MCGs. The propriety for the MCG preparation method that has been chosen is also confirmed by mass and drug content uniformity tests according to Ph.Eur.

Conflict of interest: none.

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